

### Hydrotreater Optimization

#### Catalyst performance prediction model October 2020





#### Achieve maximum performance

- Monitoring in general: know how healthy the unit is
- Evaluate effect of alternative feedstocks (cracked, VO, ...)
- Optimize performance within constraints (like cycle length)
  - Process worse feeds
  - Increase capacity
  - Reduce H<sub>2</sub> purge (when processing VO)
  - Reduce energy consumption ( $H_2$ /oil, P, ...)
- Support Troubleshooting activities
- Predict remaining cycle length
  - Evaluate Options to extend cycle length





#### Co-processing vegetable oil

 $\begin{array}{c} CH_2 = 0 - CO - C_{17}H_{33} \\ CH = 0 - CO - C_{17}H_{33} \\ I \end{array} \xrightarrow{3H_2} \begin{array}{c} CH_2 = 0 - CO - C_{17}H_{35} \\ CH = 0 - CO - C_{17}H_{35} \\ CH = 0 - CO - C_{17}H_{35} \end{array}$  $CH_2 - O - CO - C_{17}H_{33}$  $CH_2 - O - CO - C_{17}H_{35}$  $3H_2$ Decarboxylation  $3C_{17}H_{35}COOH + C_3H_8$  $C_{17}H_{36} + CO_2$  $3H_2$  $H_2$ Hydrodeoxygenation Decarbonvlation  $C_{18}H_{38} + 2H_2O$  $C_{17}H_{36} + H_2O + CO$ 

- CO & CO<sub>2</sub> formed
- Purge required to remove CO & CO<sub>2</sub>
- Valuable H<sub>2</sub> lost
- Optimization required
  - Maximize HDO over decarb
  - Vary %VO in campaigns
  - Optimize within constraints





### Modeling capabilities

- Kinetic model for HDS, HDN, HDO
  - Separate model for conversion of sterically hindered sulfur species
  - N, CO and H<sub>2</sub>S inhibition considered
  - Conditions simulated from top to bottom reactor (see next slide)
  - Distinction between hydrogenation and decarboxylation of vegetable oil and animal fat
- Strong deactivation model
  - Coke deposition
  - Metal contamination
- Model to be tuned on unit data





# **CRTALYST** INTELLIGENCE Sarl Trend from top to bottom RX





#### **Predictive power**

- Alternative feeds, for instance:
  - More cracked feed with high % aromatic sulfur or high nitrogen
  - Contaminated feeds
  - Vegetable oil:
    - Impact on H<sub>2</sub> consumption, ppH<sub>2</sub> and CO inhibition of HDS reactions
    - Check on optimization H<sub>2</sub> purge (see next slide)
  - Maximize profitability within constraints





## **CATALYST** INTELLIGENCE Sarl Minimize purge when processing VO





#### Conclusions

- Model allows optimization of:
  - Economics: %cheap feeds
  - Vegetable oil operation
- Prediction of effect of processing vegetable oil or animal fat
- Strong deactivation model allowing the evaluation of alternative operating modes
- Contact Catalyst-Intelligence for more information





#### Working method

- Tune model on complete cycle from the past
  - With enough variation in feed quality & operating modes
  - Input from pilot plant data is an option
- Model current cycle  $\rightarrow$  recommendations
  - Case studies?





#### Deliverables

- Refinery provides tuning data for HP unit and Catalyst Intelligence tunes the model.
- Refinery asks specific questions about unit optimization (options they have) and Catalyst Intelligence checks what the model predicts
- Catalyst Intelligence issues a report with recommendations and schedules call to discuss
- Evaluation independent of catalyst suppliers
- Data may also be used to write ItB for new load or to evaluate future catalyst offers.





#### Contact for free quote

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